

Original article

# An effective thermal conductivity model for fractal porous media with rough surfaces

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**Abstract:**

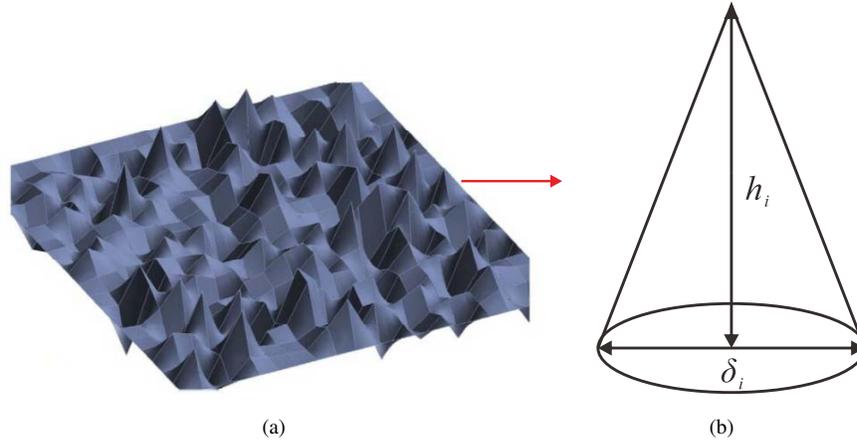
Quantitative evaluation of the effective thermal conductivity of porous media has received wide attention in science and engineering since it is a key thermophysical parameter in characterizing heat transfer properties. Based on fractal characters of tortuous capillary tubes and rough surfaces in micro-pores, we proposed a theoretical model of the effective thermal conductivity in porous media with rough surfaces. This model considers the geometrical parameters of porous media, including porosity, micro-pore fractal dimension, tortuosity fractal dimension, and relative roughness. The calculated normalized effective thermal conductivity was then validated against published experimental data. The results show good agreement between them. The influence of geometrical factors, porosity and relative surface roughness, on the effective thermal conductivity in porous media with rough surfaces are discussed and analyzed extensively.

## 1. Introduction

The effective thermal conductivity of porous media is an important property in many engineering and science applications, such as geothermal energy (Clauser, 2009), petroleum engineering (Dai et al., 2015), climate change (Kooi, 2008), and nuclear wastes (Jougnot and Revil, 2010). The effective thermal conductivity of heterogeneous porous medium is affected by the complicated relationship between the topology and geometry of pore spaces and solid matrix (Sahimi, 2011; Ghanbarian and Daigle, 2016). Thus, many effective thermal conductivity models have been proposed based on classical mixing laws. The upper and lower limits of thermal conductivity for two-phase saturated porous media corresponding to the well-known weighted arithmetic and harmonic means are generally defined by the parallel and series models (Clauser, 2009; Ranut, 2016). The Maxwell-Eucken model is often

used to characterize the thermal conductivity of porous media, where spherical pores are assumed to be widely dispersed in a continuous medium (Carson et al., 2005). The effective medium theory (EMT) is an approximated method used to model the thermal conductivity of the macroscopically homogeneous and isotropic media containing randomly distributed grains and pores (Revil, 2000; Sadeghi et al., 2018). The hybrid method is another approach to evaluate the effective thermal conductivity of porous media consisting of five basic structural models (Wang et al., 2006; Behrang et al., 2016). However, it is somewhat challenging to determine appropriate parameters for this method. In recent decades, the fractal theory has been used to study the effective thermal conductivity of porous media to account for the effect of porous media's microstructure. Yu and Cheng (2002a) proposed an effective thermal conductivity of bidispersed porous media based on fractal and thermal-electrical analogy theory. Xu et al. (2006)





**Fig. 1.** Schematic illustrations of the rough surface. (a) A real surface with the cone-shaped rough elements (Guo et al., 2015); (b) A representative cone-like rough element, where  $h$  is the height of a cone-shaped element and  $\delta$  is the base diameter of a cone-shaped element.

analyzed the effective thermal conductivity of the symmetric fractal tree-like branched networks. Pia and Sanna (2014) and Pia et al. (2016) presented an intermingled fractal model to predict the effective thermal conductivity. Shen et al. (2017) proposed an anisotropic fractal model to evaluate the effective thermal conductivity of the random metal fiber porous media. Qin et al. (2019) proposed a theoretical fractal model of effective thermal conductivity in porous media with various liquid saturation. In addition to these theoretical models, many numerical approaches such as Monte Carlo method (Wang and Li, 2017), finite element method (Li et al., 2017), and lattice Boltzmann method (Wang et al., 2007) have also been adopted to study the thermal conductivity of porous media. However, the impact of pore surface roughness has not been incorporated by mentioned above model to simulate the effective thermal conductivity.

The pore surfaces in natural porous media, in general, are rough; and the impact of roughness on thermal conductivity has been investigated extensively, primary through heat transfer measurements. Tang et al. (2007) investigated the fluid flow in stainless steel and fused silica micro-tubes experimentally. Their results indicated that the effects of surface roughness in micro-channels could not be neglected if relative surface roughness is larger than 1%. Another experiment study was carried out by Li et al. (2007) to measure the flow and heat transfer characteristics of the liquid in the smooth and rough micro-pores. They concluded that the conventional friction theory might be not useful in rough micro-pores. Majumdar and Bhushan (1990) observed that the fractal theory had the potential to describe the behavior of rough surface phenomenon. Chen and Zhang (2014) introduced the fractal Cantor structure to characterize the rough surfaces and proposed a molecular dynamics simulation to study the impact of rough surfaces on heat conduction in micro-channels. Guo et al. (2015) developed the 2D roughness model and 3D Gauss model to disclose the fluid flow and heat transfer in micro-channels with roughness. They found that both flow performance and thermal transport process were sensitive to the surface morphology. Askari et al. (2017) presented a numerical simulation of heat

conduction in a packing of particles with rough self-affine fractal surfaces.

To the best of our knowledge, the analytical expression of effective thermal conductivity in porous media with rough surfaces is rarely reported. In this study, a theoretical effective thermal conductivity model of porous media is proposed based on fractal characters of tortuous capillary tubes and rough surfaces in micro-pores. The proposed fractal model is then validated by published experimental data, and the effect of various geometrical parameters on the effective thermal conductivity of porous media are discussed in detail.

## 2. A fractal thermal conductivity model for porous media with rough surfaces

### 2.1 Fractal characteristics of rough surfaces

Some researches (Zou et al., 2008; Cai et al., 2010; Yang et al., 2014; Guo et al., 2015) showed that the rough surfaces can be described as the cone-shaped rough elements. In this study, we also assume the rough surfaces are cone-shaped and every conic peak do not overlap each other (Fig. 1). Additionally, it has been shown that the rough surfaces follow the fractal scaling law (Mahovic Poljacek et al., 2008). Thus, the base size distribution of cone-shaped elements is assumed to obey the following relationship with base diameters from  $\delta$  to  $\delta + d\delta$  (Yu et al., 2009):

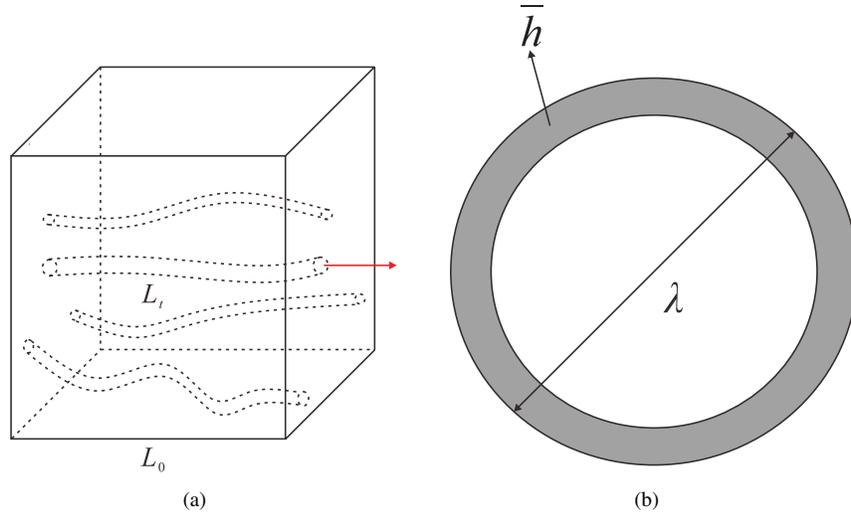
$$-dN = D\delta_{\max}^D \delta^{-(D+1)} d\delta \quad (1)$$

where  $\delta_{\max}$  is the maximum base diameter,  $D$  is the base area fractal dimension, and  $dN < 0$  implies that the number of bases decreases with increasing of the base diameter.

The base area fractal dimension  $D$  can be expressed as (Yu et al., 2009):

$$D = D_E - \frac{\ln \varphi}{\ln \alpha} \quad (2)$$

where  $D_E$  is the Euclidean dimension ( $D_E = 2$  is assumed in this study);  $\varphi$  is the ratio of the total base area of cone-shaped



**Fig. 2.** (a) The schematic illustration of the porous media composed of a bundle of tortuous micro-pores; (b) The schematic of the cross-section of a micro-pore with rough surfaces, where  $\lambda$  is the micro-pore diameter and  $\bar{h}$  is the average height of all cone-shaped elements in a micro-pore.

elements to the surface area of a micro-pore;  $\alpha = \delta_{\min}/\delta_{\max}$ ; and  $\delta_{\min}$  is the minimum base diameter.

As shown in Fig. 1, the base area of a cone-shaped element  $S_i$  can be written as:

$$S_i = \frac{\pi \delta_i^2}{4} \quad (3)$$

The volume of a cone-shaped element  $V_i$  can be expressed as:

$$V_i = \frac{1}{3} S_i h_i = \frac{\pi \delta_i^3}{12} \zeta \quad (4)$$

where  $\zeta = h/\delta$  is the ratio of the height to the base diameter of a cone-shaped element.

Based on Eqs. (1) and (3), the total base area of all cone-shaped elements  $S$  can be obtained by an integration of all diameters from  $\delta_{\min}$  to  $\delta_{\max}$ :

$$S = - \int_{\delta_{\min}}^{\delta_{\max}} S_i dN = \frac{\pi D \delta_{\max}^2 (1 - \varphi)}{4(2 - D)} \quad (5)$$

From Eqs. (1) and (4), the total volume of all cone-shaped elements  $V_t$  can be written as:

$$V_t = - \int_{\delta_{\min}}^{\delta_{\max}} V_i dN = \frac{\pi \zeta D \delta_{\max}^3 (1 - \alpha^{3-D})}{12(3 - D)} \quad (6)$$

The surface area of a micro-pore  $S_t$  can be expressed as:

$$S_t = \frac{S}{\varphi} = \frac{\pi D \delta_{\max}^2 (1 - \varphi)}{4(2 - D)\varphi} \quad (7)$$

Combining Eqs. (6) and (7), the average height of all cone-shaped (rough) elements  $\bar{h}$  can be given as:

$$\bar{h} = \frac{V_t}{S_t} = \frac{\zeta \varphi \delta_{\max} (2 - D) (1 - \alpha^{3-D})}{3(3 - D) (1 - \varphi)} \quad (8)$$

The porous media is often considered to be composed of a bundle of tortuous micro-pores (see Fig. 2), whose size

distribution follows the fractal scaling law (Cai et al., 2014). Thus, the micro-pore diameter  $\lambda$  distribution has a similar relationship with Eq. (1):

$$-dN = D_f \lambda_{\max}^{D_f} \lambda^{-(D_f+1)} d\lambda \quad (9)$$

where  $\lambda_{\max}$  is the maximum micro-pore diameter,  $D_f$  is the micro-pore fractal dimension.

The micro-pore fractal dimension  $D_f$  also can be expressed as:

$$D_f = D_E - \frac{\ln \phi}{\ln \beta} \quad (10)$$

where  $\phi$  is the porosity,  $\beta = \lambda_{\min}/\lambda_{\max}$  and  $\lambda_{\min}$  is the minimum micro-pore diameter.

The relative roughness  $\gamma$  can be defined by (Yang et al., 2015):

$$\gamma = \frac{2\bar{h}}{\lambda} \quad (11)$$

It is assumed that the micro-pores in porous media have identical relative roughness. Thus, Eq. (11) can be rewritten as:

$$\frac{(h_{\max})_{\lambda_{\min}}}{(h_{\max})_{\lambda}} = \frac{\lambda_{\min}}{\lambda} \quad (12)$$

where  $(h_{\max})_{\lambda_{\min}}$  is the maximum height of cone-shaped element in the minimum micro-pore and  $(h_{\max})_{\lambda}$  is the maximum height of cone-shaped element in a micro-pore.

Inserting Eqs. (8) and (12) into Eq. (11), the relative roughness  $\gamma$  can be rewritten as:

$$\gamma = \frac{2\varphi (h_{\max})_{\lambda_{\min}} (2 - D) (1 - \alpha^{3-D})}{3\lambda_{\min} (3 - D) (1 - \varphi)} \quad (13)$$

Eq. (13) indicates that the relative roughness in the rough micro-pores is related to geometrical parameters. Thus, each parameter in Eq. (13) has a physical meaning.

### 2.2 Fractal model for effective thermal conductivity of porous media with rough surfaces

Based on the classical Fourier's law and the thermal-electrical analogy method, the thermal resistance of a single tortuous capillary tube with rough surfaces  $r_f$  can be expressed as (Miao et al., 2016):

$$r_f = \frac{4L_t}{\pi k_f (\lambda - 2\bar{h})^2} = \frac{4L_t}{\pi k_f \lambda^2 (1 - \gamma)^2} \quad (14)$$

where  $L_t$  is the actual length of fluid path and  $k_f$  is the thermal conductivity of fluid. The actual length of fluid path is given by (Yu and Cheng, 2002b):

$$L_t = \lambda^{1-D_T} L_0^{D_T} \quad (15)$$

where  $L_0$  is the characteristic length along the direction of heat flow and  $D_T$  is the tortuosity fractal dimension for micro-pore.

The relationship between the fractal dimension characteristic length  $L_0$  and the total cross-sectional area  $A$  can be expressed by:

$$L_0 = \sqrt{A} \quad (16)$$

The total cross-sectional area  $A$  can be determined by (Cai et al., 2012):

$$A = \frac{\pi D_f \lambda_{\max}^2 (1 - \phi)}{4(2 - D_f)\phi} \quad (17)$$

The tortuosity fractal dimension for micro-pore can describe the tortuous degree of the capillary tubes in porous media quantitatively. This specific microstructural parameter of  $D_T$  is difficult to determine experimentally, but can be calculated through an approximate formula (Wei et al., 2015):

$$D_T \approx (D_E - D_f + 1) + (D_E - D_f) \frac{\log D_f - \log(D_f - 1)}{\log \phi} \quad (18)$$

As the capillary tubes considered to be parallel, the total thermal resistance of fluid in rough micro-pores  $R_f$  can be obtained as:

$$\frac{1}{R_f} = - \int_{\lambda_{\min}}^{\lambda_{\max}} \frac{1}{r_f} dN \quad (19)$$

Inserting Eqs. (9), (14), and (15) into Eq. (19), the total thermal resistance of fluid in rough micro-pores can be given as:

$$R_f = \frac{4L_0^{D_T} (D_T - D_f + 1)}{\pi k_f D_f \lambda_{\max}^{D_T+1} \left(1 - \phi^{\frac{D_T - D_f + 1}{2 - D_f}}\right) (1 - \gamma)^2} \quad (20)$$

The thermal resistance of solid matrix  $R_s$  can be written as:

$$R_s = \frac{L_0}{(1 - \phi) A k_s} \quad (21)$$

where  $k_s$  is the thermal conductivity of solid matrix.

The effective thermal conductivity of porous media with rough surfaces  $k_e$  can be expressed as:

$$k_e = \frac{L_0}{R_t A} = \frac{L_0}{A} \left( \frac{1}{R_f} + \frac{1}{R_s} \right) \quad (22)$$

Finally, based on Eqs. (16), (17), (20) and (21), Eq. (22) of the effective thermal conductivity of porous media with rough surfaces can be obtained as:

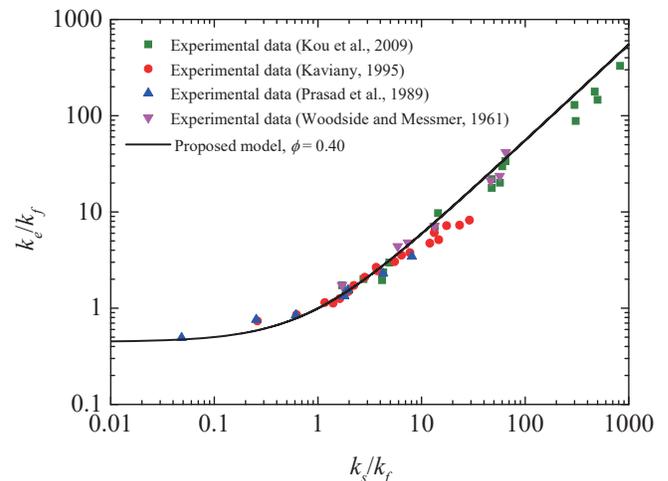
$$k_e = \frac{k_f (2 - D_f) \phi \left(1 - \phi^{\frac{D_T - D_f + 1}{2 - D_f}}\right) \left(\frac{\lambda_{\max}}{L_0}\right)^{D_T - 1}}{(D_T - D_f + 1)(1 - \phi)} (1 - \gamma)^2 + (1 - \phi) k_s \quad (23)$$

Eq. (23) is a function of porosity ( $\phi$ ), fractal dimension of the micro-pore ( $D_f$ ), tortuosity fractal dimension of the micro-pore ( $D_T$ ), characteristic length ( $L_0$ ), maximum micro-pore diameter ( $\lambda_{\max}$ ), relative roughness ( $\gamma$ ), and the thermal conductivity of the solid matrix and fluid. This proposed theoretical model reveals the physical basis of heat transfer in porous media with rough surfaces.

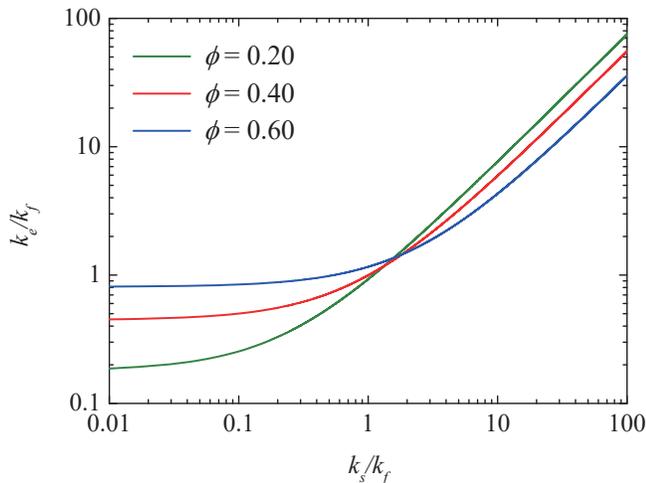
### 3. Results and discussion

In this section, we first compare the results from our proposed model with various experimental measurements from other available literature. Then, we discuss the sensitivity of the proposed model to their parameters, such as porosity and relative roughness.

Fig. 3 presents the comparison between the proposed model prediction and experimental data for saturated porous media with porosity of 0.4 (Woodside and Messmer, 1961; Prasad et al., 1989; Kaviany, 1995; Kou et al., 2009). Some researches (Feng et al., 2007; Miao et al., 2016) have found that the  $\lambda_{\min}/\lambda_{\max}$  ratio is usually in the range of  $10^{-2} \sim$



**Fig. 3.** The comparison between proposed model prediction and experimental data for saturated porous media when the porosity equals to 0.40, where  $\alpha = 0.01$ ,  $\beta = 0.01$ ,  $2(\lambda_{\max})_{\lambda_{\min}}/\lambda_{\min} = 0.1$  and  $\phi = 0.2$ .

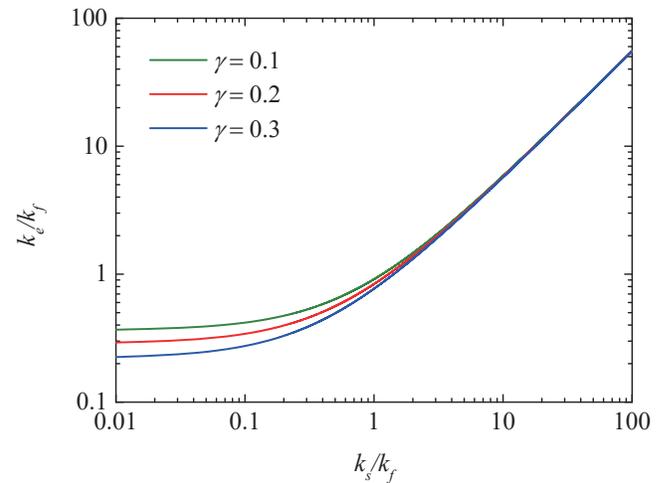


**Fig. 4.** The dimensionless effective thermal conductivity versus the thermal conductivity ratio of the solid phase to fluid phase at different porosity, where  $\alpha = 0.01$ ,  $\beta = 0.01$ ,  $2(h_{\max})_{\lambda_{\min}}/\lambda_{\min} = 0.1$  and  $\phi = 0.2$ .

$10^{-4}$  in many natural porous media. Thus,  $\alpha = 0.01$  and  $\beta = 0.01$  are applied to this study. As the maximum height of the cone-shaped element to the micro-pore diameter is in the range of  $0.12 \sim 0.17$  (Li et al., 2003),  $2(h_{\max})_{\lambda_{\min}}/\lambda_{\min} = 0.1$  is assumed in this study. The ratio of the total base area of cone-shaped elements to the surface area of a micro-pore is  $\phi = 0.2$  (Cai et al., 2014). As can be seen in Fig. 3, the proposed model prediction is in good agreement with the available experimental data.

Fig. 4 shows the dimensionless effective thermal conductivity versus the thermal conductivity ratio of the solid phase to the fluid phase at a different porosity. It is seen that the dimensionless effective thermal conductivity increases as the porosity decreases when the thermal conductivity ratio of the solid to fluid phases  $k_s/k_f > 1$ . On the contrary, if  $k_s/k_f < 1$ , the dimensionless effective thermal conductivity increases with the increase of the porosity. This can be explained by the fact that the volume fraction of the solid phase with higher thermal conductivity increases, leading to an increase of the effective thermal conductivity when  $k_s/k_f > 1$ . Whereas, when  $k_s/k_f < 1$ , the result is opposite. These results are analogous to those given by Miao et al. (2016).

Fig. 5 illustrates the dimensionless effective thermal conductivity versus the thermal conductivity ratio of the solid phase to the fluid phase at a different relative roughness when the porosity equals 0.40. It is observed that the dimensionless effective thermal conductivity decreases with the increasing the relative roughness. This may be attributed to the effect on the heat transfer in micro-pores as the increase of the thermal resistance which is consistent with the result given by Askari et al. (2017). In addition, it is found that the dimensionless effective thermal conductivity is slightly dependent on the relative roughness when  $k_s/k_f > 10$ . It implies that the effect of surface roughness in micro-pores may be neglected if the thermal conductivity of solid matrix much larger than the con-



**Fig. 5.** The dimensionless effective thermal conductivity versus the thermal conductivity ratio of the solid phase to fluid phase at a different relative roughness when the porosity equals 0.40.

ductivity of fluid.

#### 4. Conclusions

In this work, the analytical expression for the effective thermal conductivity of porous media with rough surfaces is derived based on the fractal geometry theory. The effective thermal conductivity is a function of microstructural parameters, such as porosity, micro-pore fractal dimension, tortuosity fractal dimension for micro-pore, and relative roughness. The present model predictions show a good agreement with published experimental data of various natural and engineered materials. This newly proposed model allows the physical understanding of thermal transport in porous media with rough surfaces.

It should be noted that the theoretical model proposed in this study only focuses on the effect of the surface roughness in micro-pores and pore size distributions on the heat conduction in porous media. The model can be improved by considering the self-affine fractals in micro-pores and the varying relative roughness in different micro-pores. Also, thermal transport in natural porous media involves convection and radiation that has not been considered in this study.

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